

Backstepping Control of Stefan Problem with Flowing Liquid

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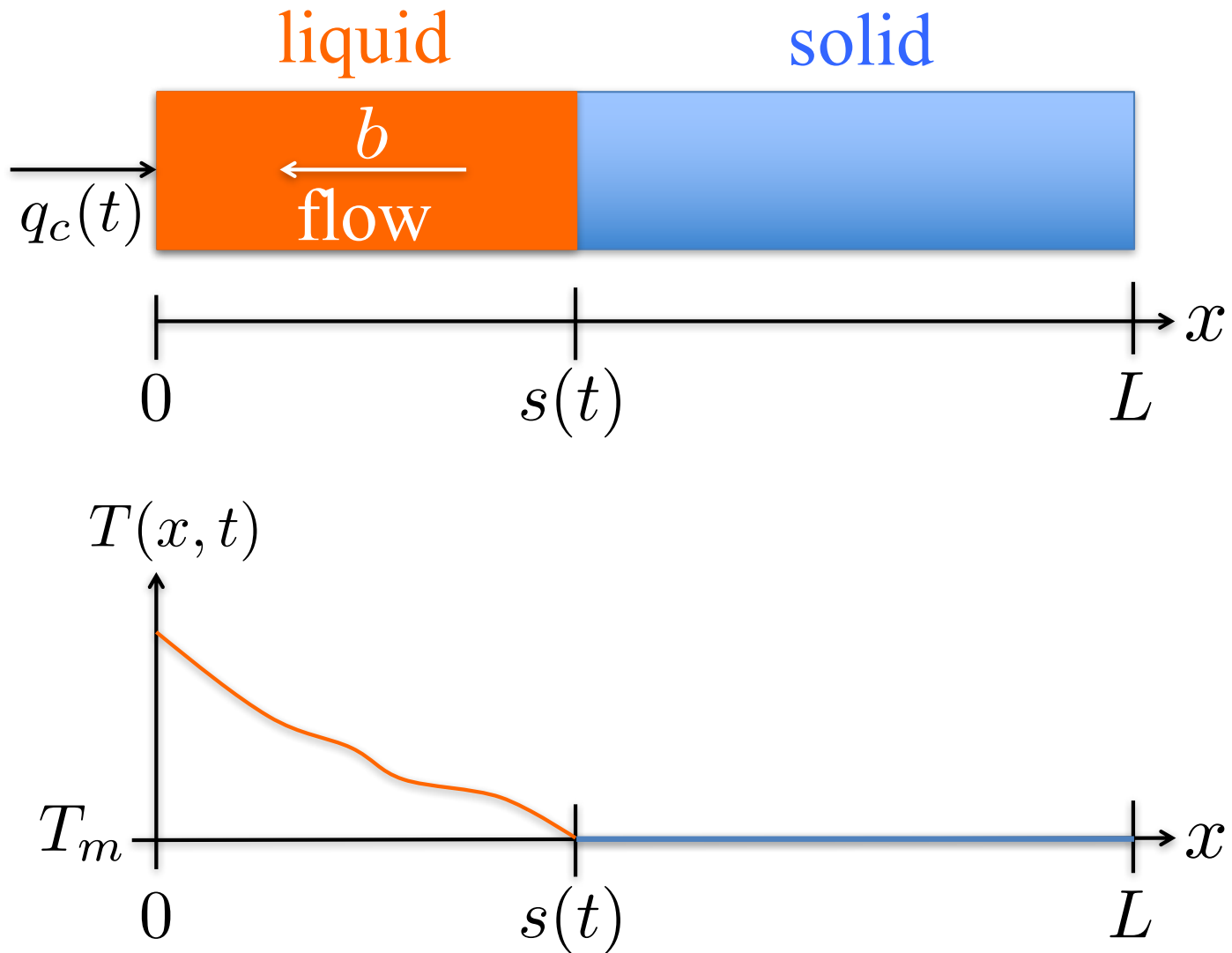
ACC 2017

Outline

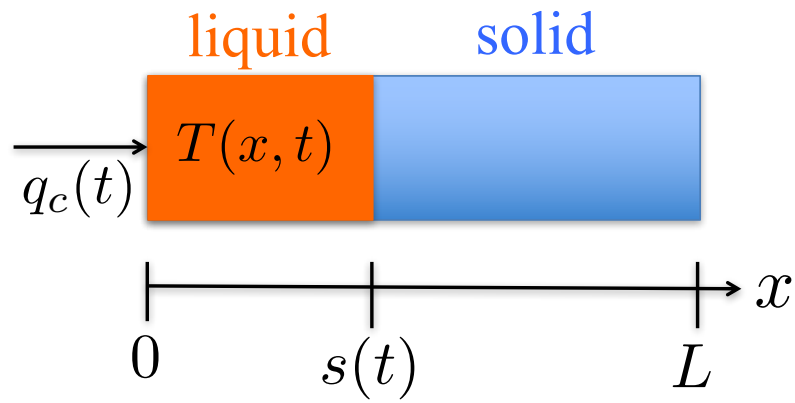
- Problem Statement
- Control Design
- Simulation & Future Work

Problem Statement

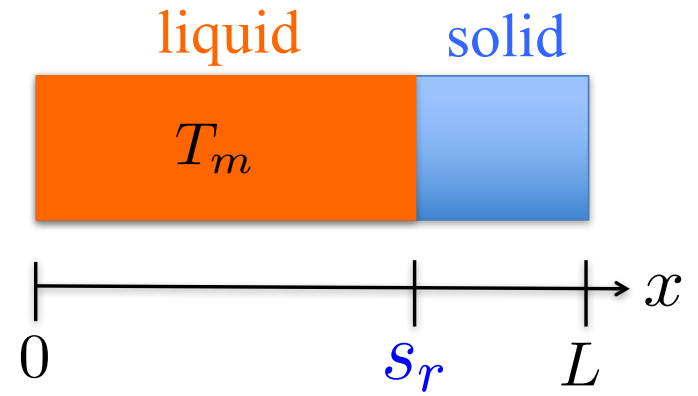
Physical Model : Melting + Flow



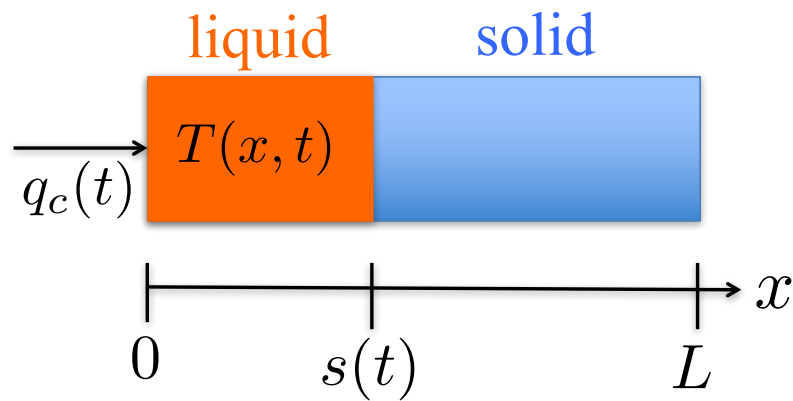
During the process



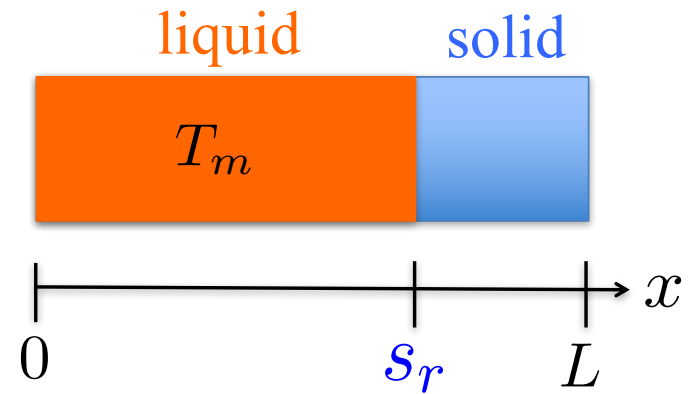
Desired state



During the process

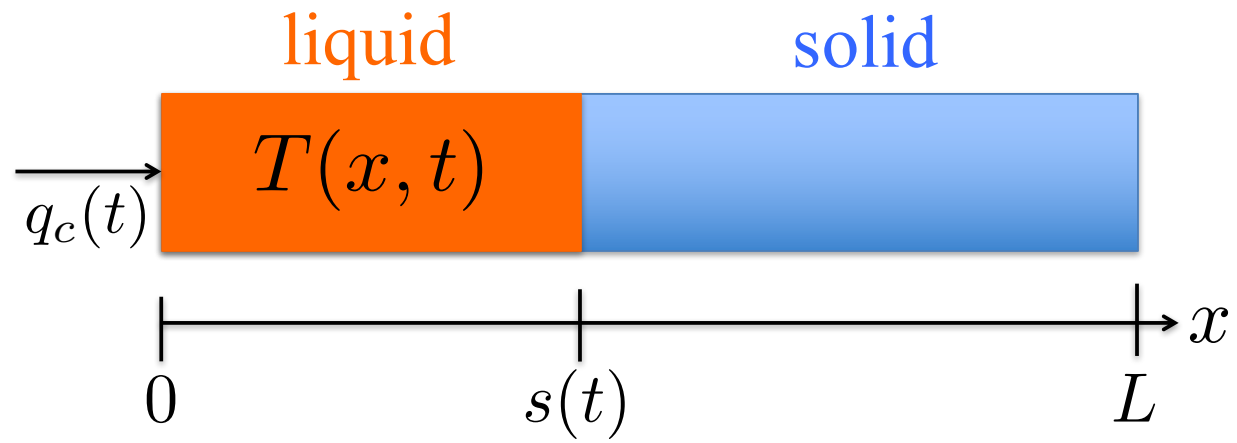


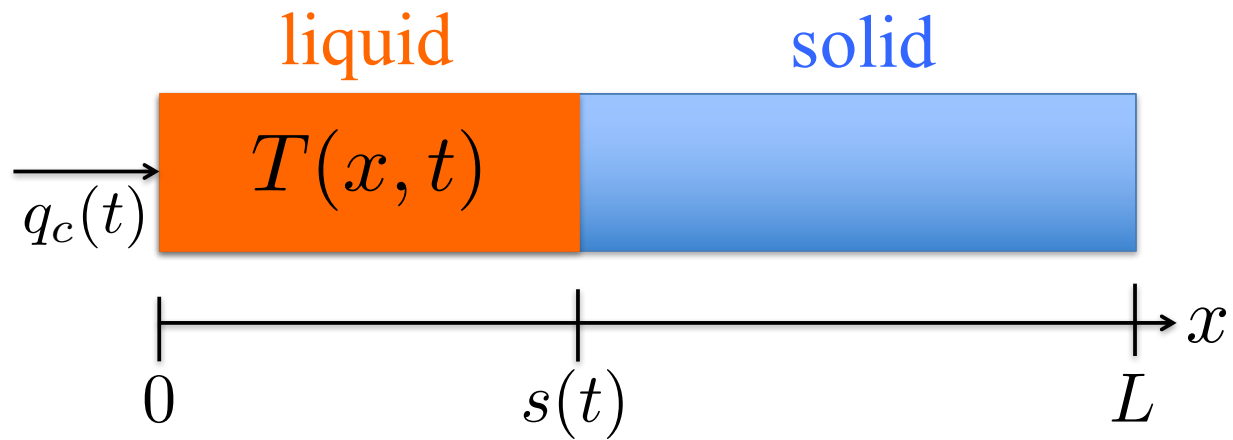
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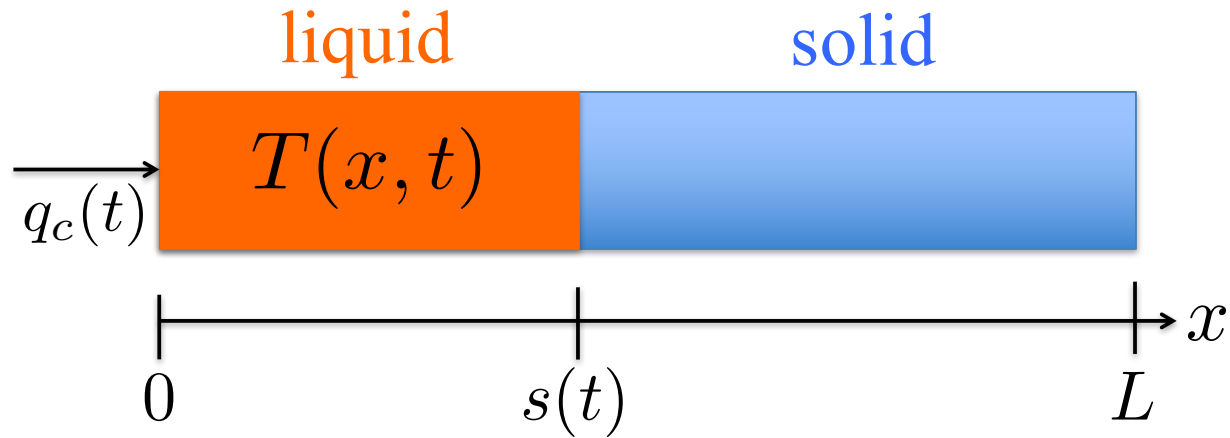
Objective: Design heat control $q_c(t)$ to achieve

$$s(t) \rightarrow s_r, \quad T(x, t) \rightarrow T_m, \quad \text{as } t \rightarrow \infty$$

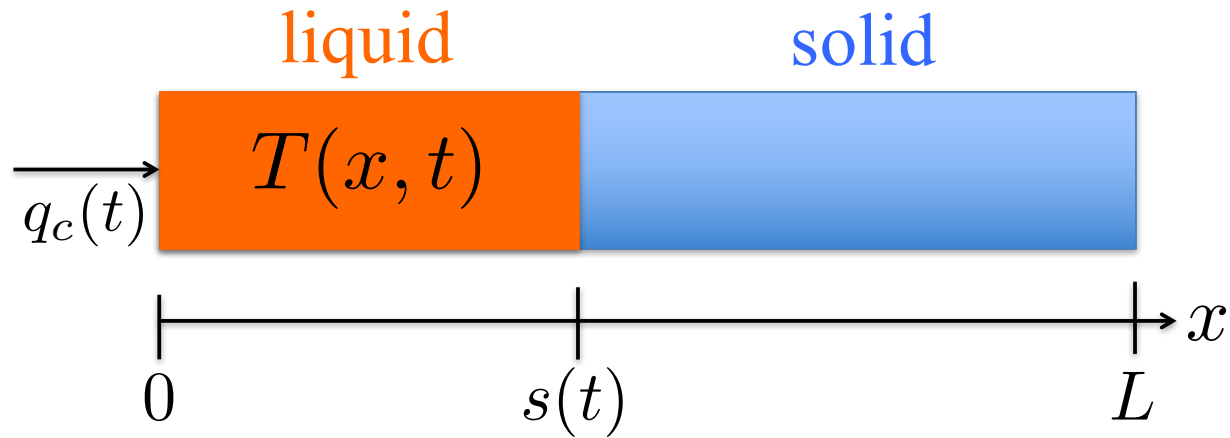




PDE $T_t(x, t) = \alpha T_{xx}(x, t) + bT_x(x, t), \quad 0 < x < s(t) < L$



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 $T_x(0, t) = -q_c(t)/k$
 $T(s(t), t) = T_m$

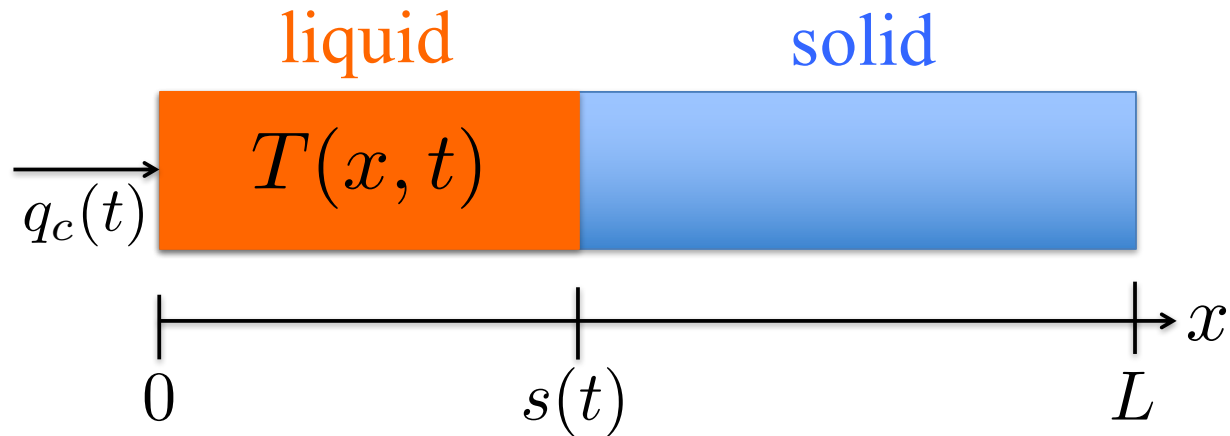


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ODE $\dot{s}(t) = -\beta T_x(s(t), t)$



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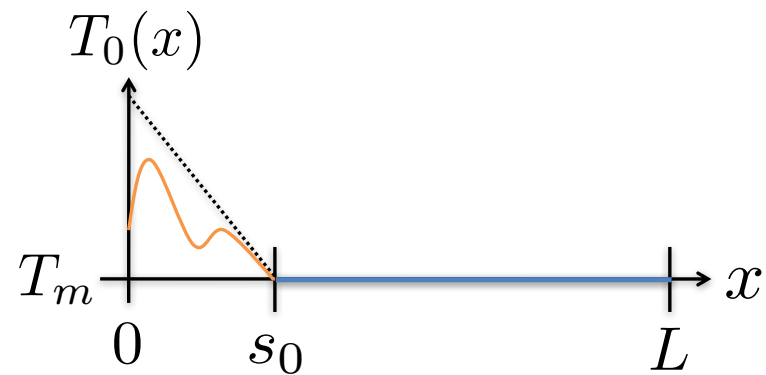
$$T(s(t), t) = T_m$$

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State-dependent moving boundary \rightarrow Nonlinear

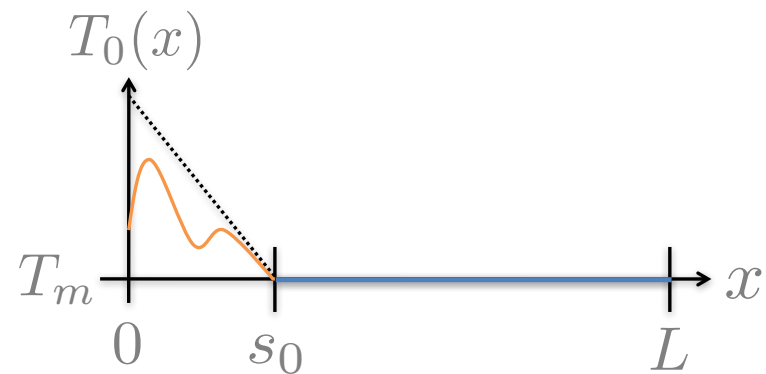
Assumption : Initial interface position $s_0 > 0$, and initial temperature $T_0(x)$ is Lipschitz ($H := \text{Lip. const.}$)

$$0 < T_0(x) - T_m < H(s_0 - x)$$



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Remark : Model valid iff

$$T(x, t) > T_m, \quad \text{for } \forall x \in (0, s(t)), \quad \forall t > 0$$

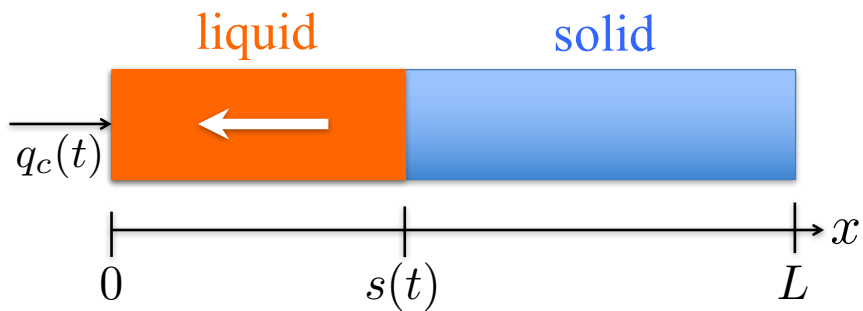
Energy Conservation

$$\frac{d}{dt} \left(\frac{1}{\alpha} \int_0^{s(t)} (T(x, t) - T_m) dx + \frac{1}{\beta} s(t) \right) = \frac{q_c(t)}{k} - \frac{b}{\alpha} (T(0, t) - T_m)$$

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- Counter-convection $b > 0$

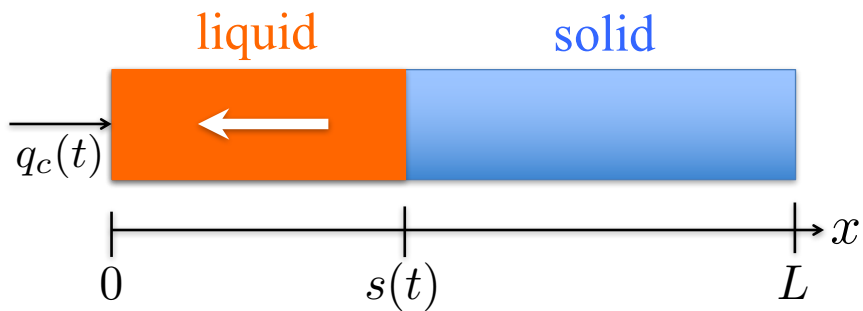


Neutralizes the energy growth

Energy Conservation

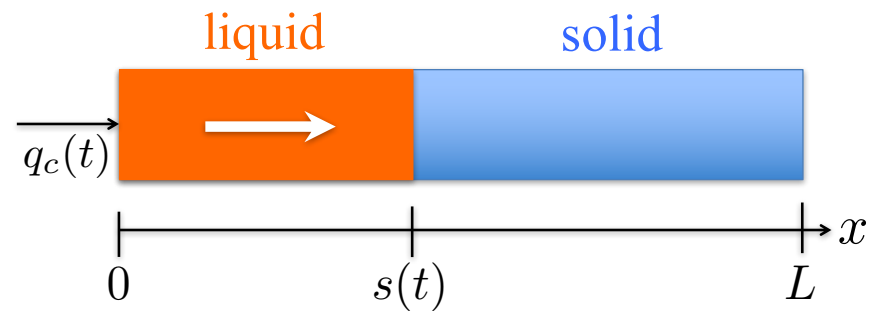
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Neutralizes the energy growth

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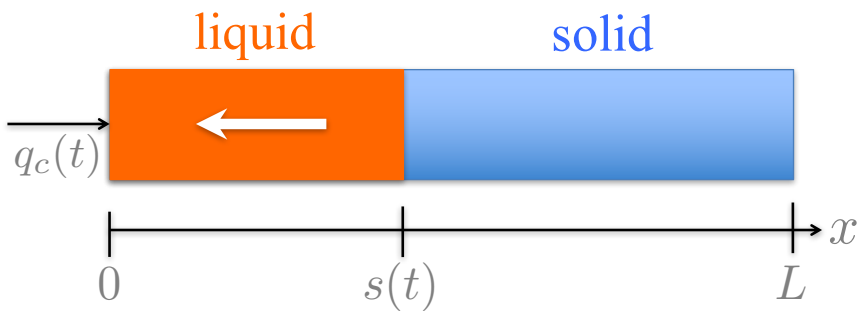


Promotes the energy growth

Energy Conservation

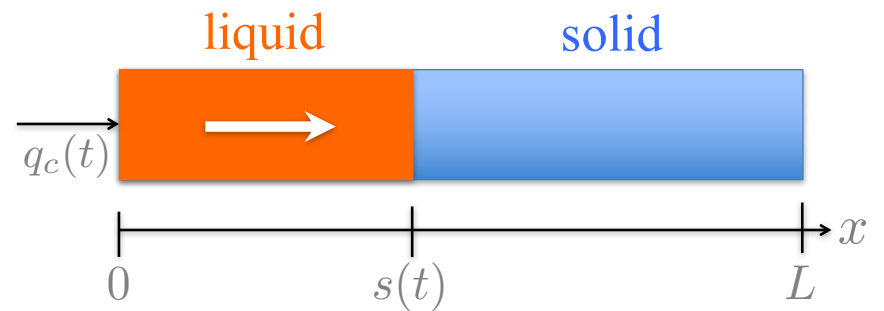
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Neutralizes the energy growth

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Promotes the energy growth

Intuition : s_r should be chosen sufficiently far from s_0 depending on $T_0(x)$ and b .

Main Results

Theorem 1 [Counter-convection]

Suppose $b > 0$. Consider the control law

$$q_c(t) = \frac{kb}{2\alpha}(T(0, t) - T_m) - ck \left(\frac{1}{\alpha} \int_0^{s(t)} \cosh\left(\frac{b}{2\alpha}x\right) e^{\frac{b}{2\alpha}x} (T(x, t) - T_m) dx + \frac{2\alpha}{b\beta} \cosh\left(\frac{b}{2\alpha}s(t)\right) \left(e^{\frac{b}{2\alpha}s(t)} - e^{\frac{b}{2\alpha}s_r} \right) \right),$$

Then, for any s_r verifying **setpoint restriction**

$$s_r > s_0 + \frac{2\alpha}{b} \ln \left(1 + \frac{b\beta}{2\alpha^2} \int_0^{s_0} (T_0(x) - T_m) dx \right),$$

the setpoint (T_m, s_r) is exponentially stable in \mathcal{H}_1 -norm.

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Note : As $b \rightarrow \infty$, the restriction is relaxed to $s_r > s_0$.

Theorem 2 [Regular-convection]

Suppose $b < 0$. Consider the same control law as counter-convection.

Assume $(T_0(x), s_0)$ satisfy **initial condition requirement**

$$\int_0^{s_0} (T_0(x) - T_m) dx < \frac{2\alpha^2}{\beta|b|} e^{-\frac{|b|}{2\alpha}s_0}.$$

Then, for any s_r verifying **setpoint restriction**

$$s_r > s_0 - \frac{2\alpha}{|b|} \ln \left(1 - \frac{|b|\beta}{2\alpha^2} e^{\frac{|b|}{2\alpha}s_0} \int_0^{s_0} (T_0(x) - T_m) dx \right),$$

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	$b > 0$	$b = 0$	$b < 0$
I.C. Requirement	None	None	Temp. cool
Setpoint Restriction	Less than ★	★	More than ★

Control Design

Change of variables

Reference errors

$$u(x, t) = (T(x, t) - T_m) e^{\frac{b}{2\alpha}x}, \quad X(t) = \frac{2\alpha}{b} \left(e^{\frac{b}{2\alpha}s(t)} - e^{\frac{b}{2\alpha}s_r} \right).$$

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(u, X) -system

$$\text{PDE} \quad u_t(x, t) = \alpha u_{xx}(x, t) - \lambda u(x, t), \quad 0 < x < s(t)$$

$$u_x(0, t) = -U(t), \quad u(s(t), t) = 0,$$

$$\text{ODE} \quad \dot{X}(t) = -\beta u_x(s(t), t),$$

where

$$\lambda := \frac{b^2}{4\alpha}, \quad U(t) := \frac{q_c(t)}{k} - \frac{b}{2\alpha}(T(0, t) - T_m).$$

Model validity

Lemma If $U(t) > 0$ $\forall t > 0$, then $u(x, t) > 0$ & $\dot{s}(t) > 0$ for $\forall x \in (0, s(t))$
 $\forall t > 0$ which verifies

$$T(x, t) > T_m, \forall x \in (0, s(t)), \forall t > 0$$

Proof is by maximum principle

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$$T(x, t) > T_m, \forall x \in (0, s(t)), \forall t > 0$$

Proof is by maximum principle

Lemma With $b > 0$ (counter-convection), $U(t) > 0$ implies $q_c(t) > 0$.

Note : With $b < 0$ (regular-convection), $U(t) > 0$ *does not ensure* $q_c(t) > 0$.

Design Procedure

- Backstepping transformation

$$w(x, t) = u(x, t) - \frac{\beta}{\alpha} \int_x^{s(t)} \phi(x - y) u(y, t) dy - \phi(x - s(t)) X(t),$$

where $\phi(x) = \frac{c}{\beta} \sqrt{\frac{\alpha}{\lambda}} \sinh\left(\sqrt{\frac{\lambda}{\alpha}} x\right)$.

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- Target (w, X) -system

PDE $w_t(x, t) = \alpha w_{xx}(x, t) - \lambda w(x, t) + \dot{s}(t) \phi'(x - s(t)) X(t),$
 $w_x(0, t) = 0, \quad w(s(t), t) = 0,$

ODE $\dot{X}(t) = -cX(t) - \beta w_x(s(t), t),$

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ODE $\dot{X}(t) = -cX(t) - \beta w_x(s(t), t),$

- Control design (*nonlinear*)

$$U(t) = -c \left(\frac{1}{\alpha} \int_0^{s(t)} \cosh \left(\sqrt{\frac{\lambda}{\alpha}} x \right) u(x, t) dx + \frac{1}{\beta} \cosh \left(\sqrt{\frac{\lambda}{\alpha}} s(t) \right) X(t) \right)$$

Proposition Provided $U(0) > 0$, the followings hold

$$\begin{array}{ll} U(t) > 0, & * q_c(t) > 0 \text{ with } b > 0 \\ u(x, t) > 0, \quad \dot{s}(t) > 0, & * \text{model valid for both } b \\ s_0 < s(t) < s_r, & * \text{no overshoot for both } b \end{array}$$

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Lemma Target (w, X) -sys. is *exp. stable* with $\dot{s}(t) > 0$ & $s_0 < s(t) < s_r$.

Proof : Lyapunov analysis

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Lemma Target (w, X) -sys. is exp. stable with $\dot{s}(t) > 0$ & $s_0 < s(t) < s_r$.

Proof : Lyapunov analysis



Lemma (T, s) -sys. is *exp. stable* at the setpoint (T_m, s_r) .

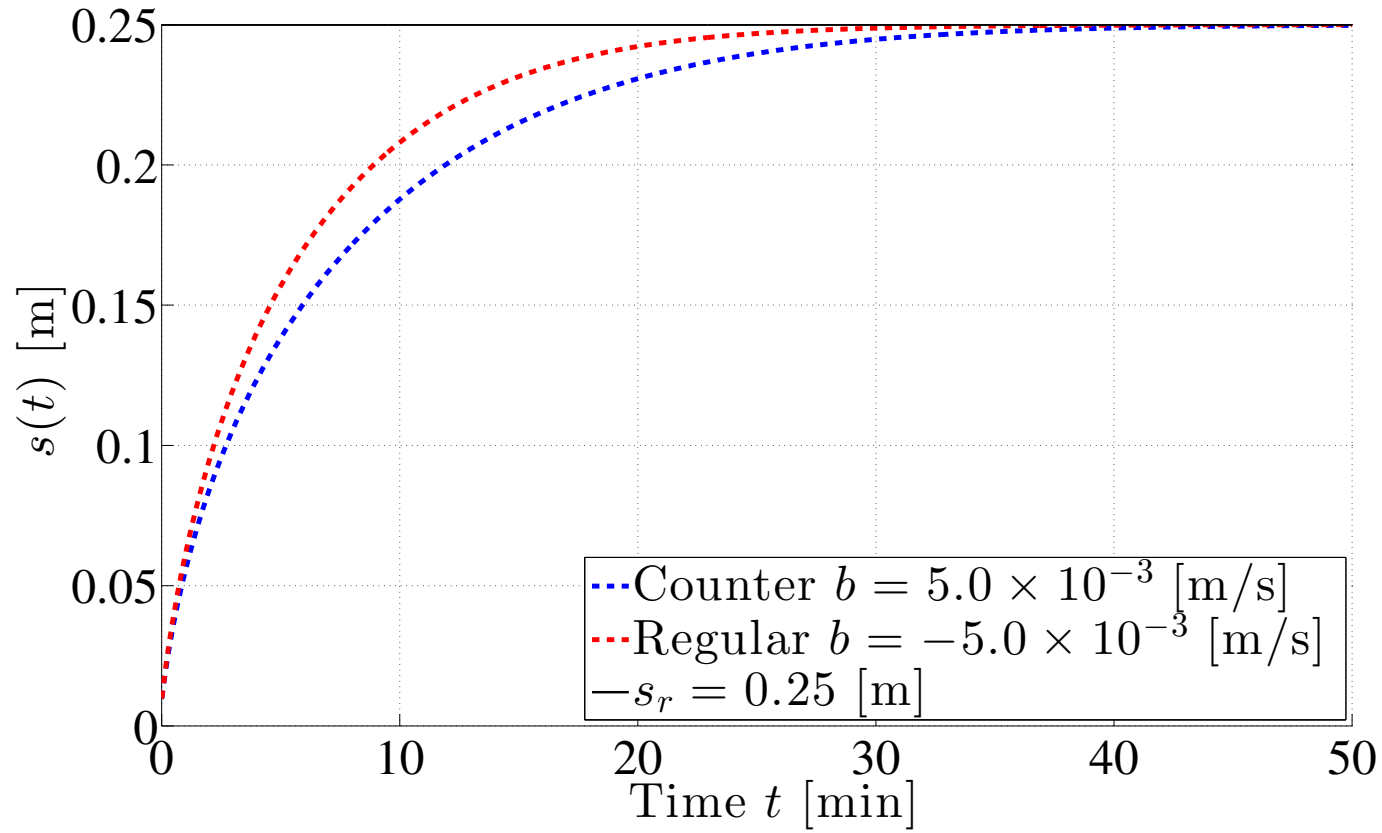
Proof : Invertibility of transformations with $s_0 < s(t) < s_r$

Concludes the theorems.

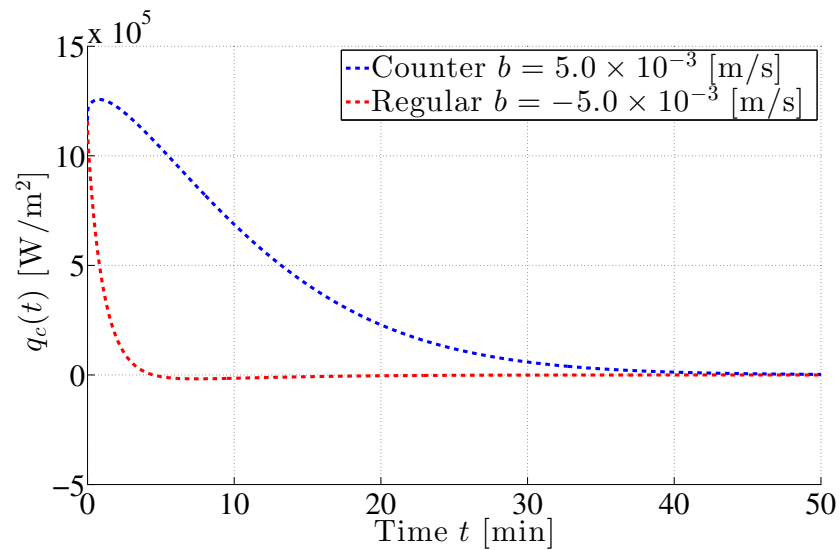
Simulation & Future Work

Numerical Simulation

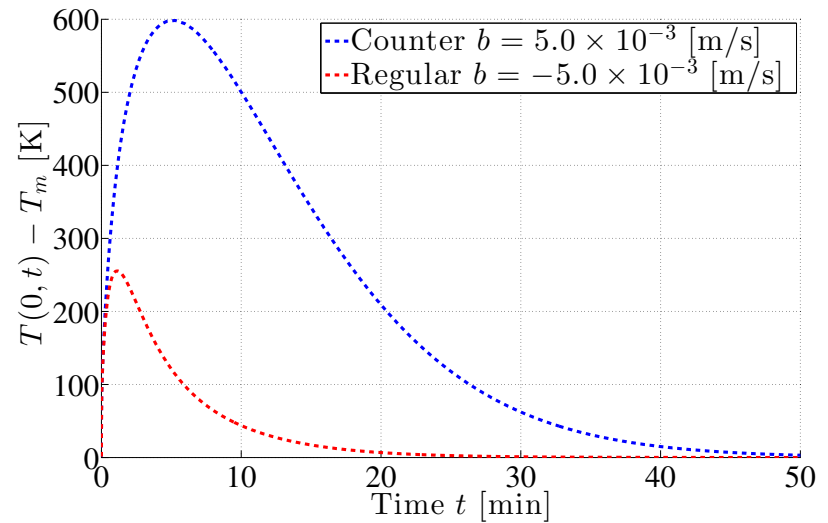
Zinc



* No overshoot



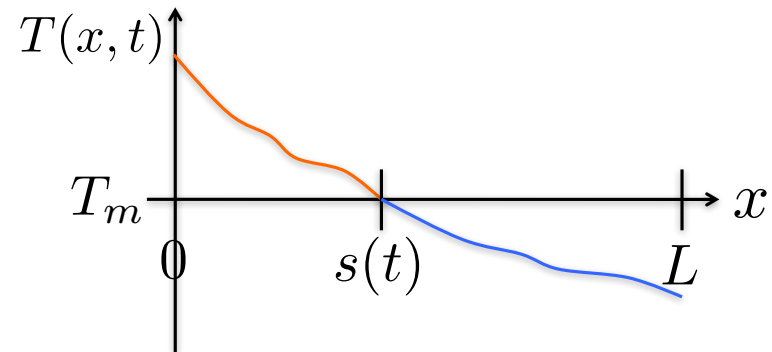
* Positive heat with $b > 0$,
while with $b < 0$ it can be negative.



* Temperature warms up
and cool into melting point.

Future Work

- Two-phase Stefan problem



- Extrusion for 3D-printing

